ANAN'YEV, M.G.; VAYNRIB, Ye.A.; VISHNEVSKIY, A.A.; KOZLOV, Yu.G.; LEVITSKAYA, L.A.; MARTYNOV, L.N.; MUSHEGYAN, S.A.; FRID, Ye.A.

Improvement of the artificial heart apparatus designed by the Scientific Research Institute of Experimental Surgical Apparatus and Instruments. Eksper.khir. 4 no.5:3-8 S-0 '59. (MIRA 13:1)

1. Iz Nauchno-issledovatel skogo instituta eksperimental noy khirurgicheskoy apparatury i instrumentov (dir. M.G. Anan'yev) i Instituta khirurgii imeni A.V. Vishnevskogo (dir. - deystvitel'nyy chlen AMN SSSR A.A. Vishnevskiy) AMN SSSR (HEART, MECHANICAL, equipment and supplies)

VAYNRIB, Ye.A.; MARTYNOV, L.N.; FRID, Ye.A.; KOZLOV, Yu.G.; ANAN YEV, M.G.; MUSHEGYAN, S.A.; LEVITSKAYA, L.A.

Apparatus for artificial blood circulation. Med.prom. 14 no.11:40\_45 N '60. (MIRA 13:11)

1. Mauchno-issledovatel\*skiy institut eksperimental\*noy khirurgicheskoy apparatury i instrumentov.

(BLOOD -- CIRCULATION, ARTIFICIAL) (MEDICAL INSTRUMENTS AND APPARATUS)

ANAN'YEV, M.G.; VAYNRIB, Ye.A.; KOZLOV, Yu.G.; LEVITSKAYA, L.A.; MARTYMOV,
L.N.; MUSEGYAN, S.A.; FRID, Ye.A.

Improved apparatus for artificial blood circulation (the AIK of 1959)
and new data on its use. Trudy NIIERHAI no.5:113-118 '61.

1. Nauchno-issledovatel'skiy institut eksperimental'noy khirurgicheskoy apparatury i instrumentov.

(PERFUSION PUMP (HEART))

TRAPEZNIKOV, N.N.; AVDEYEVA, I.A.; MUSHEGYAN, S.A.; LEVITSKAYA, L.A.

Experimental basis of chemotherapy of malignant tumors of the extremities by the method of regional perfusion. Vest.ANN SSSR 17 no.6:67-72 '62. (MIRA 15:8)

1. Institut eksperimental'noy i klinicheskoy onkologii AMN SSSR i Institut eksperimental'noy khirurgicheskoy apparatury i instrumentov Ministerstva zdravookhraneniya SSSR.

(EXTREMITIES (ANATOMY)—CANCER) (CHEMOTHERAPY) (PERFUSION PUMP (HEART))

APPROVED FOR RELEASE: 03/13/2001 CIA-RDP86-00513R001135720003-9"

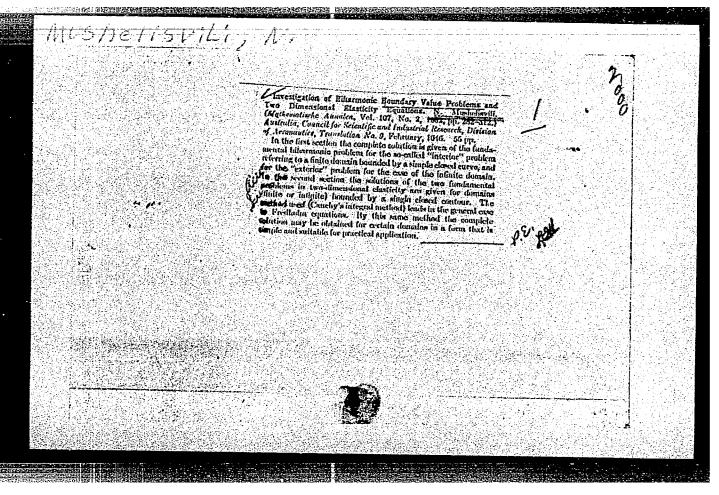
YAVORSKIY, V.V.; MUSHECYAN, S.A.; TRAPEZNIKOV, N.N.

Experimental and clinical bases for using the extracorporeal circulation apparatus AIX.PN-62 for regional perfusion. Eksp. khir. 1 anest. 8 no.5:16-19 S.D '63. (MIRA 17:6)

MUSHEGYAN, J.A.; G RIMTEN, J.V.; HARTES V, J.A.; HYPER, N.A.

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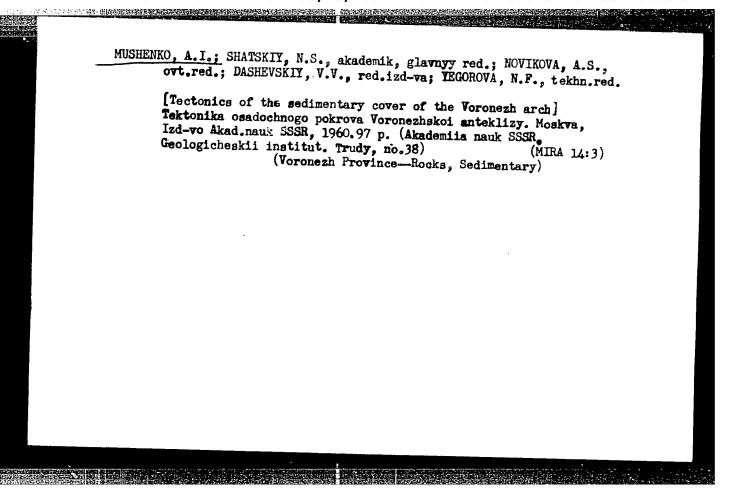
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Source: Mathematica)	l Reviews, 1950	Vol 11 No. g	(mil pa	
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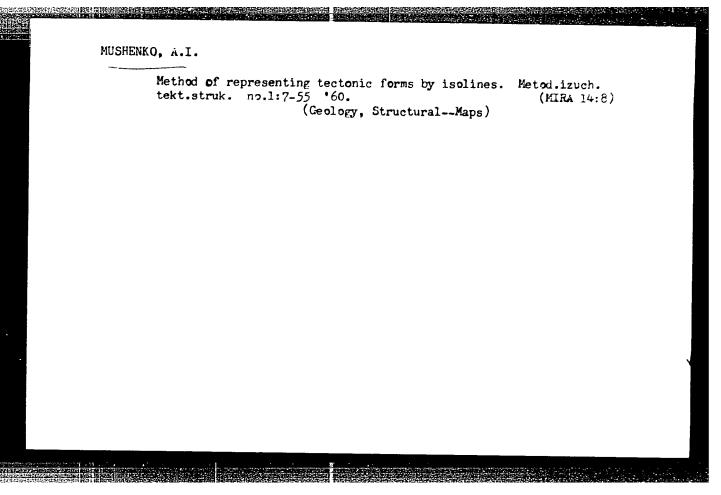
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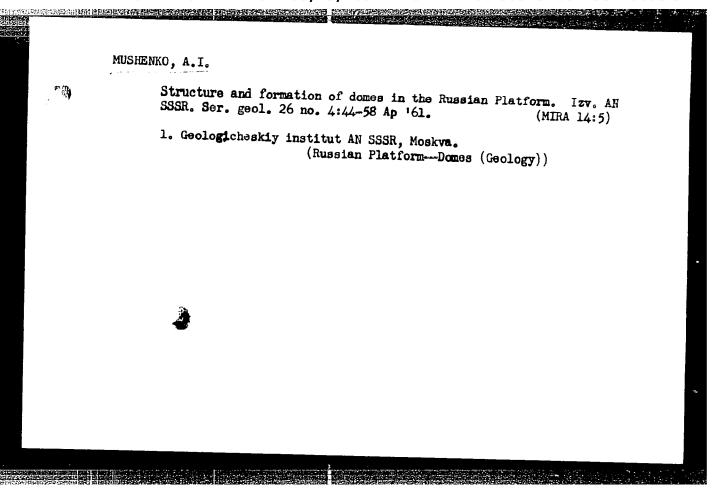
AUTHOR: Mushenko, A.I. SOV/5-59-5-3/20 TITLE: The Tectonics of the Sedimentary Blanket Deposit of the Voronezh Anteclize (Tektonika osadochnogo pokrova Voronezhskoy anteklizy) PERIODICAL: Byulleten Moskovskogo obshchestva ispytateley prirody, Otdel geologicheskiy, 1958, Nr 5, pp 38 - 51 (USSR) ABSTRACT: The Voronezh anteclize was formed by Paleozoic and Mesozoic layers of sedimentary rocks, which with a sharp unconformity angle, cover the ancient mostly-dislocated and metamorphized Pre-Cambrian crystalline foundation. The diversity of these rocks in different parts of the anteclize indicates that these parts were formed under different geological conditions. The author gives a very detailed description of the anteclize and of the conditions which governed the accumulation of sedimentary layers. He finds that the formation of the anteclize in the Paleozoic and Mesozoic eras was caused by two sinking zones connected with the anteclize the Moscow syneclize and the Dnepr-Donets depression The Card 1/2 following geologists are mentioned by the author: A.D. Arkh-

SOV/5-59-5-3/20
The Tectonics of the Sedimentary Blanket Deposit of the Voronezh Anteclize angel skiy, N.S. Shatskiy, A.A. Dubyanskiy, D.N. Sobolev, V.N. Sobolevskaya, V.N. Preobrazhenskaya, and V.A. Zhukov. There are 4 maps, 2 profiles and 18 Soviet references

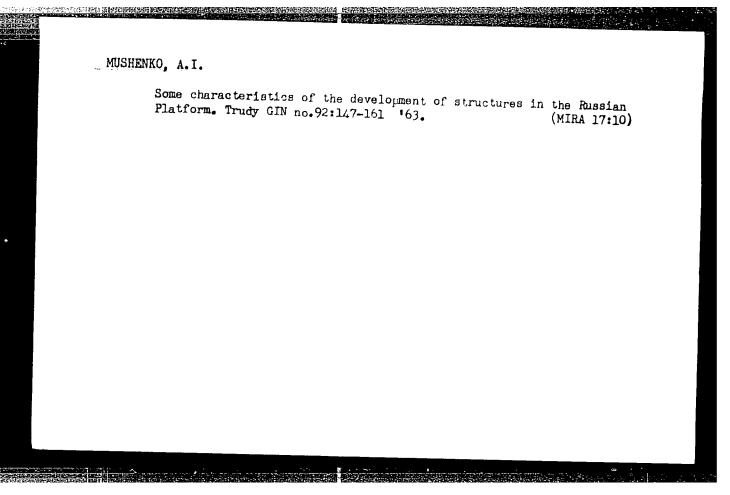
Card 2/2







# MUSHENKO, A.I. Structure of the eastern slope of the Moscow syneclise. Lok1, AN SSSR 142 no.3:655-656 Ja \*62. (MiRa 15:1) 1. Geologicheskiy institut AN SSSR. Predstavleno akademikom A.L. Yanshinym. (Moscow region--Geology, Structural)



# MUSHENKO, A.I.

Inversions of tectonic movements in the Russian Platform. Geotektonika no.1:22-34 Ja-F '66. (MIRA 19:1)

1. Geologicheskiy institut AN SSSR.

MUSHENKÓ, D.V.

USSR/Chemical Technology. Chemical Products and Their

Application -- Treatment of natural gases and

petroleum. Motor fuels. Lubricants.

Abs Jour: Ref Zhur-Khimiya, No 3, 1957, 9310

Author Katsman, S. V. and Mushonko, D. V.

Inst Not given

Titlo The Reactions of Some High-Molecular Hydrocarbons

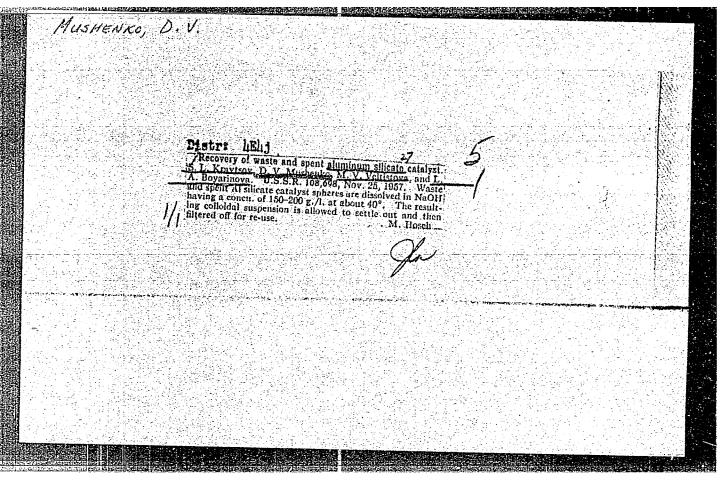
with Stoam

Zh. prikl. khimii, 1956, Vol 29, No 6, 955-957 Orig Pub:

Abstract: The reaction of n-docano, bonzone, naphthalone, and 124 -methyl-naphthalone with steam over an industrial Ni-catalyst, used in the treatment of

methane to produce H<sub>2</sub> /sic/, has been investigated. The catalyst was activated by treatment with H<sub>2</sub> for two hours at 700°. The gaseous products from the decomposition of the hydrocarbons contain about 70% H<sub>2</sub> and 10-20% CO<sub>2</sub> and CO. The ratio CO<sub>2</sub>:CO increases as the temperature is

Card 1/2



AUTHORS:

Mayorev, D. M. and Mushenke, D. V. 307/65-58-6-5/13

TITLE:

Hydrogenation of  $C_{10} - C_{16}$  Acros to Alsohels (Gidrirevaniye kislot  $C_{10} - C_{16}$  v spirty)

PERIODICAL:

Khimiya i Tekhnologiya Topliv i Masel, 1958. Nr.6. pp. 24 - 29 (USSR).

ABSTRACT:

Primary high-molecular aliphatic alcohols and 3.75 of their derivatives have recently gained increasing importance in the USSR as well as abroad. Work parried out in the USA, UK, and France is reviewed. In 1956 the authors investigated the hydrogenation of  $c_{10}$  -  $c_{10}$ acids to the corresponding alcohols. The acids were obtained from the Shebekino Combine SZhK. Their properties and composition are tabulated. Distillation was carried out on a 15-plate vacuum restification solumn. A laboratory continuous circulation plant was used for tests at 200 - 300 atms pressure for 30 - 450 hours with 200 - 400 ml of acpper chromate tatalyst. The raw materials and the hydrogenate were analysed for their acid number, saponification number, quantity of non-saponified matter and water content. In the non-saponified part the content of hydrocarbons and alcohols was determined chromatographically. It could

Card 1/2

Hydrogenation of  $c_{10} = c_{16}$  Actes to Alder its. Similar 65 88.6.8713

be seen that with increasing temperature the dorth of conversion of acids increases from 19%- 79% (Table 1) and that the alcohol and hydroparton content in the hydrogenate increases sharply. At pressurer of 300 atms and a ratio of hydrogen to raw material equalling 200:1 much greater rates of conversion of the acid with apprepriate yields of the products could be achieved (Table 2). Experiment 36 was carried out to investigate conditions for increasing the yield of alcenols and for decreasing the yield of hydroparbons. Conditions of this test as well as characteristics and composition of the hydrogenate are tabulated. Samples of sodium salts of alkyl sulphonates were tested for their detergent properties and experiments using these alcohols for synthesizing high quality oil additives were carried out by members of the VNIINP. The corresion resistance of various metals to fatty acids was tested (Taries 3 and 4); chemically pure Al and Ni, and some types of stainless steel, were found to have the highest porresion resistance. There are 4 Tables and 8 References: I French, 3 English, 1 Japanese and 3 Scriet.

Card 4/4

ASSOCIATION: LenNII

OTHER BEACHES AND A SECOND OF THE SECOND OF

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67040

AUTHORS:

Vishnevskiy, N. Ye. Mushenko, D. V.

SOV/153-2-5-25/31

TITLE:

Extraction of Isobutylene From the Butane-butylene Fraction

PERIODICAL:

Izvestiya vysshikh uchebnykh zavedeniy. Khimiya i khimicheskaya

tekhnologiya, 1959, Vol 2, Nr 5, pp 779 - 783 (USSR)

ABSTRACT:

In the course of producing butyl-sulfuric acid from the cracking gases, the isobutylene contained in the butane-butylene fraction, is not only completely polymerized but it also draws the n-butylene into the copolymerization. This reduces the yield in secondary butyl alcohol. It was established in 1957 at the Institute of the authors (formerly LenNII, Leningradskiy nauchno-issledovatel skiy institut po pererabotke nefti i polucheniyu iskusstvennogo shidkogo topliva - Leningrad Scientific Research Institute for Processing Petroleum and Producing Synthetic Liquid Fuels) that the mentioned raw material may, at the most, contain 26 of isobutylene. Therefore, the surplus isobutylene must previously be extracted when using this method. One variant of the reaction of A. M. Butlerov (Refs 1-4) was reproduced by Standard Oil in 1942 (Ref 5), and they obtained a 1.26-content of isobutylene. There is no information on the design of the equipment for the reaction and on the capacity of the reaction space. The authors achieved

Card 1/3

SOV/153-2-5-25/31

Extraction of Isobutylene From the Butane-butylene

the isobutylene extraction from the mentioned fraction with a method of two-step counterflow and 65% sulfuric scid. The duration of contact was 9 minutes per step. This short duration was achieved due to the isothermal reaction occurring because of intensive stirring (Ref 6, Fig 2). This reduced the the hotens. ficulties in a high degree. The raw material was the butane-butvlene fraction from the Lumberstakiv Detwolous Defiance butylene fraction from the Lyuberetskiy Petroleum Refinery. Table 1 contains the results of experiments. Neither a decrease Table | contains the results of experiments, welther a decrease of temperature from 450 to 3000, nor an additional one to 250 = 35000, nor additional one to 250 = 35000, applying a 70% H<sub>2</sub>SO<sub>4</sub> increased the extraction (Table 2), but the content of isobutylene in the final product increased to content of isoputylene in the final product increased to 1.4 mol/mol H<sub>2</sub>SO<sub>4</sub>. Therefore the optimum conditions of extraction are: 45°C, pressure 10 atm, ratio between raw material and H2SO4 9: 1, initial concentration of isobutylene 10%, final concentration 2%, duration of contact 10 minutes per step. Figure 1 shows the dependence of the Saturation degree of sulfuric acid on the isobutylene concentration, Thus, the main characteristic factors of the two-step process can be observed. Table 3 shows

card 2/3

Praction

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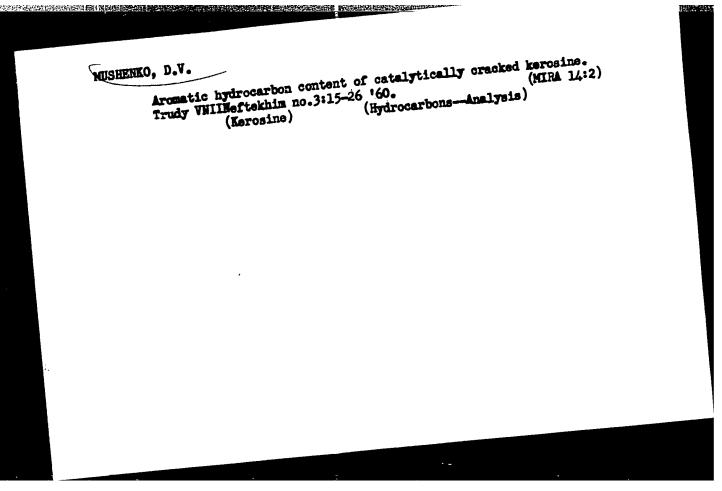
Extraction of Isobutylene From the Butane-butylene Fraction

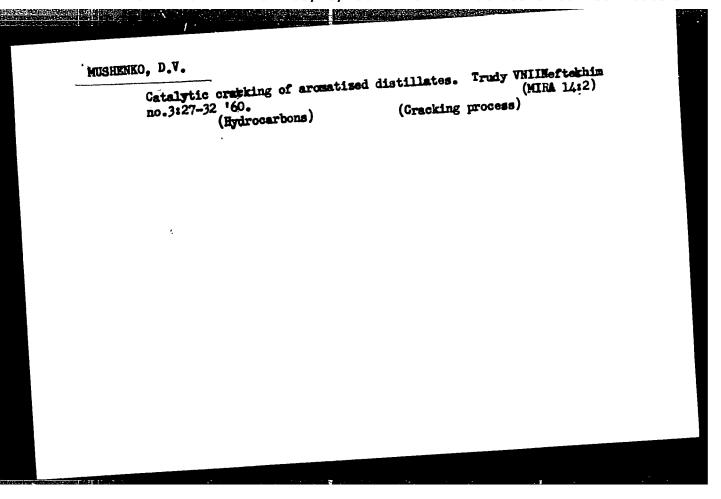
SOV/153-2-5-25/31

the experimental data of the extraction method described. They are in accordance with the theoretical explanations. The results of the second step even surpass them. From the data in table 2 it follows that approximately 65% of the isobutylene passes over into the acid layer in each step. From a raw material containing about 10-12% isobutylene, approximately 80% of its potential is extracted. Its content in the concentrate is 96%. A method of extraction of isobutylene with 40% sulfuric acid, developed by Professor M. S. Nemtsov et al. from the Vsesoyuznyy nauchnoissledovatel'skiy institut sinteticheskogo kauchuka (All-Union Scientific Research Institute of Synthetic Rubber) is E tioned in the article. There are 2 figures, 3 tables, and 6 references, 5 of which are Soviet.

ASSOCIATION: Vsesoyuznyy nauchno-issledovateliskiy institut neftekhimicheskikh protsessov - VNIINEFTEKHIM (All-Union Scientific Research Institute of Petroleum-chemical Processes - VNIINEFTEKhim)

Card 3/3





s/081/61/000/011/024/040 B103/B202 Repeated catalytic cracking ("tandem cracking") of kerosene Mushenko, D. V. AUTHOR: Referativnyy zhurnal. Khimiya, no. 11, 1961, 479 - 480, of direct distillation abstract 11M 167(11M167). ("Tr. Vses. n.-i. in-t neftekhim. TITLE: protsessov", 1960, vyp. 3, 33 - 35) TEXT: It was the aim of this paper to obtain data on successive, catalytic PERIODICAL: cracking of distillates in order to check the expediency of recirculation cracking or distillates in order to check the expediency of recticulation of kerosene of intermediate fractions. For this purpose catalytic cracking of kerosene or direct distillation of Kalinskaya petroleum was carried out five times successively on a laboratory apparatus at 450°C, at a volume rate of 0.7, under atmospheric pressure, on a catalyst with an activity index of 34. gasoline boiling up to 200°C was separated from each catalyzate obtained and the residue was subjected to cracking under the same conditions. It was the residue was subjected to cracking under the same conditions. It was demonstrated that in each of the successive cracking cycles the gasoline Card 1/2

s/081/61/000/011/024/040 B103/B202

and gas yield decreases, the coke yield increases, and the quality of the Repeated catalytic cracking... gasoline becomes considerably poorer. The benzine obtained by cracking kerosene from direct distillation contains the following hydrocarbons in %: unsaturated 18.3, aromatic 24.4, paraffins 36.5, naphthene 22.9 and after unsaturated 10.7, aromatic 24.4, parallins 70.7, naphthene 22.7 and after the fifth cracking cycle: 71.1; 2.4; 23.0; 2.9. The increase in aromatic hydrocarbons in the raw material in each successive cracking cycle (from 11.00) and 11.00 21.8% in kerosene of direct distillation to 61.8 % in the raw material of the fifth cycle) leads to a considerable deterioration of the technological indices of the process. It is concluded that recirculation of the intermediate fractions in catalytic cracking without previous pregaration intermediate fractions in catalytic cracking without previous preparation of the recirculating product is inexpedient. [Abstracter's note: Complete translation.

Card 2/2

\$/081/61/000/013/014/028 B110/B205

AUTHORS:

Mushenko, V. M., Mushenko, D. V.

TITLE:

Effect of unsaturated hydrocarbons on the antiknocking

characteristics of aviation gasolines

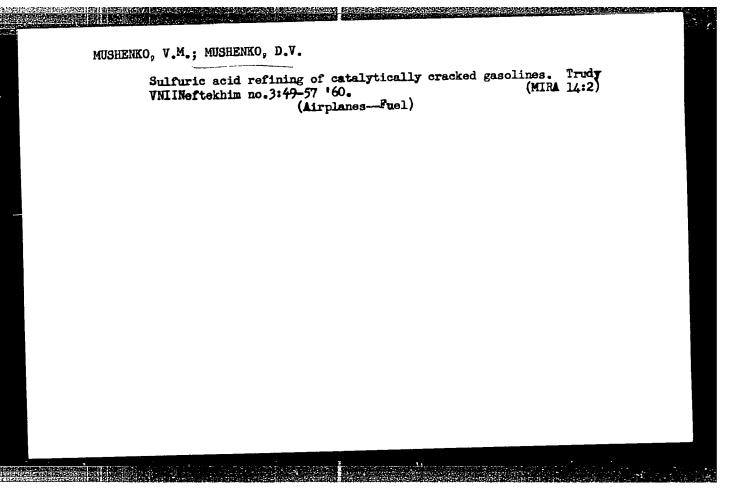
PERIODICAL:

Referativnyy zhurnal. Khimiya, no. 13, 1961, 524, abstract 13M278 (Tr. Vses. n.-i. in-t neftekhim. protsessov, 1960,

vyp. 3, 44-48)

TEXT: The authors studied the effect of admixtures of amylenes, obtained by dehydration of isoamylene alcohol, on the octane numbers of mixtures of **5**-70(B-70) gasoline with commercial isooctane and of catalytically cracked gasoline. On the basis of the studies performed it was recommended to add 5-20% of the commercial pentane - amylene fraction to aviation gasolines obtained by direct distillation in order to increase their octane numbers by 1-3. [Abstracter's note: Complete translation]

Card 1/1



24830 s/081/61/000/011/037/040 B110/B201

5.3300

Mushenko, V. M., Mushenko, D. V.

: RAOFTUA

Antiknocking properties of aviation gasoline from

TITLE:

catalytic cracking

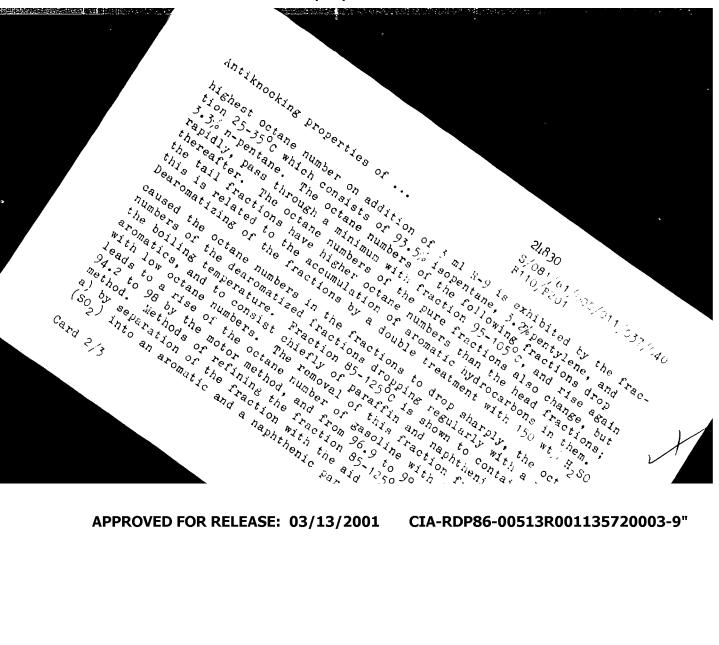
Referativnyy zhurnal. Khimiya, no. 11, 1961, 486, abstract 11M219 (11M219) (Tr. Vses. n.-i. in-t neftekhim. protsessov,

PERIODICAL: TEXT: A study has been made of the antiknocking properties of fractions obtained by distillation on the Gadaskin column and two-stage treatment (catalytic cracking and purification of the typical aviation component of Kalinskoye gas oil (Baku). The properties of initial gasoline were

 $d_A^{20} = 0.7418$ ; initial boiling point = 48°C; boiling out of 97.5. at 4 168°C; chemical Froup composition in 70: olefins = 3.1; aromatics = 34.2; paraffins = 49.4; naphthenes = 13.0. Octane number (motor method) in pararrins = 47.4; maphonenes = 7.0. Octane number (motor motor) and pure form = 81.4; with 3 ml P-9 (R-9) per kg = 94.2. A study of the pure rorm = 01.4; wrom j mr 6-7 (n-2) per no = 74.2. A Study of the the antiknocking properties of the fractions of this gasoline showed that the

Card 1/3

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24830 s/081/61/coc/611/037/046 B110/E201

Antiknocking properties of ...

highest octane number on addition of 3 ml R-9 is exhibited by the fraction 25-35°C which consists of 93.5% isopentane, 3.2% pentylene, and 3.3% n-pentane. The octane numbers of the following fractions drop rapidly, pass through a minimum with fraction 95-105°C, and rise again thereafter. The octane numbers of the pure fractions also change, but the tail fractions have higher octane numbers than the head fractions; this is related to the accumulation of aromatic hydrocarbons in them. Dearomatizing of the fractions by a double treatment with 150 wt, H<sub>2</sub>SO<sub>4</sub>

caused the octane numbers in the fractions to drop sharply, the octane numbers of the dearomatized fractions dropping regularly with a rise of the boiling temperature. Fraction  $85-125^{\circ}\mathrm{C}$  is shown to contain little aromatics, and to consist chiefly of paraffin and naphthenic hydrocarbons with low octane numbers. The removal of this fraction from the gasoline leads to a rise of the octane number of gasoline with 3 ml R-9 from 94.2 to 98 by the motor method, and from 96.9 to 99.1 by the 1-C (1-S) method. Methods of refining the fraction  $85-125^{\circ}\mathrm{C}$  are suggested: a) by separation of the fraction with the aid of a selective solvent  $(SO_2)$  into an aromatic and a naphthenic paraffin part, and subsequent

Card 2/3

24830

Antiknocking properties of ...

S/081/61/060/011/037/046 B110/B201

introduction of aromatics into the gasoline; b) catalytic reforming. The latter is the most expedient way of improving the octane number of this fraction. Catalytic reforming on aluminum-molybdenum catalysts permits 80% aviation gasoline with the octane number 89 to be obtained in pure state (motor method). Addition of a reformed substance to the remaining fractions allows gasoline  $\frac{100}{130}$  (B 100/130) to be produced without alkylate addition. [Abstracter's note: Complete translation.]

Card 3/3

MUSHENKO, D.V.; KATSMAN, S.V.; TSELLINSKAYA, T.F.

Catalytic cracking of the primary products of synthesis. Trudy VNIINeftekhim no.3:70-87 '60. (MIRA 14:2)

(Cracking process)

S/081/61/000/011/025/040 B103/B202

AUTHORS:

Mushenko, D. V., Mochalovskaya, A. P.

TITLE:

Catalytic cracking of distillates with increased nitrogen content

PERIODICAL:

Referativnyy zhurnal. Khimiya, no. 11. 1961, 480, abstract 11 M 170(11M170). ("Tr. Vses. n.-i. in-t neftekhim. protsessov", 1960, vyp. 3, 8S - 90)

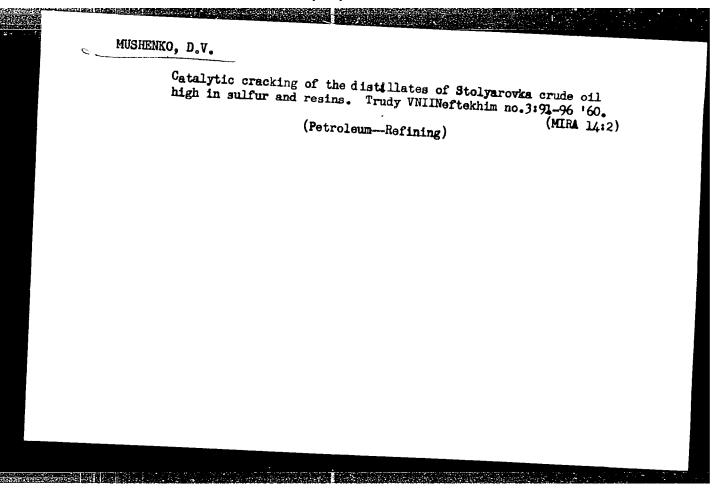
TEXT: The authors present results of experiments with catalytic cracking of gas oils by means of hydrogenation in liquid phase of the Stolyarovskiy masut containing 1.8 - 2.0 wt % of nitrogen bases. Cracking at a standard 22 - 23 %, at a VR of 1.5 the yield decreases to 15 - 16 %. The unsatisfactory results of the cracking of gas oils cannot be explained by the composition of their hydrocarbons but are apparently due to the poisoning the removal of the nitrogen bases from the gas oil sample their cracking Card 1/2

Catalytic cracking of distillates...

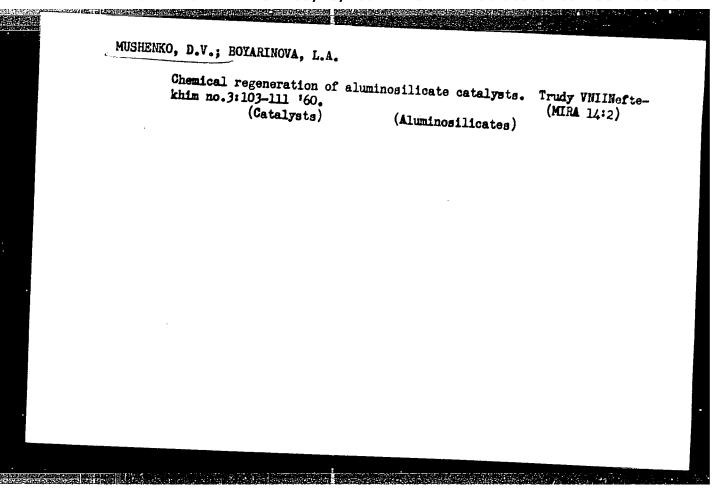
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yielded 29.4 % gasoline at a VR = 0.7 and 25.2% at a VR = 1.5. A 50 % yield is achieved with a raw material containing bases at a VR = 0.51 and a raw material without bases at a VR = 0.68. Hence the removal of bases this case is 1.2 times higher and the coke yield is 2/3 as compared to the Complete translation. Abstracter's note:

Card 2/2



Cat the	Catalytic cracking of gas oils in the presence of propylene and of the propane-propylene fraction. Trudy VNIINeftekhim no.3:97-102 '6				
	(Gracking process)	(MIRA 14:2)			
•					



Determination of fluorine in an aluminosilicate catalyst and in alumina by hydrolysis with superheated steam. Trudy VNIINeftekhim no.3:112-115 '60. (MIRA 14:2)

(Fluorine—Analysis) (Aluminosilicates)

(Alumina)

KATSMAN, S.V.; MUSHENKO, D.V.; TEREBILOVA, M.A.

Contact coking and catalytic cracking of fuel oil from Tuymazy
Devonian oil. Trudy VNIINeftekhim no.3:116-141 '60. (MIRA 14:2)

(Petroleum as fuel)

MUSHENKO, D.V.; MOCHALOVSKAYA, A.P.

Contact coking and catalytic cracking of Stolyarova crude oil high in sulfur and resins. Trudy VNIINeftekhim no.3:142-149 '60.

(Petroleum as fuel)

(Petroleum as fuel)

S/081/61/000/012/022/028 B103/B202

AUTHOR:

Mushenko, D. V.

TITLE:

Contact coking of mazout on activated carbon

PERIODICAL:

Referativnyy zhurnal. Khimiya, no. 12, 1961, 524, abstract 12**M**165. (Tr. Vses.n.i. in-t neftekhim. protsessov, 1960,

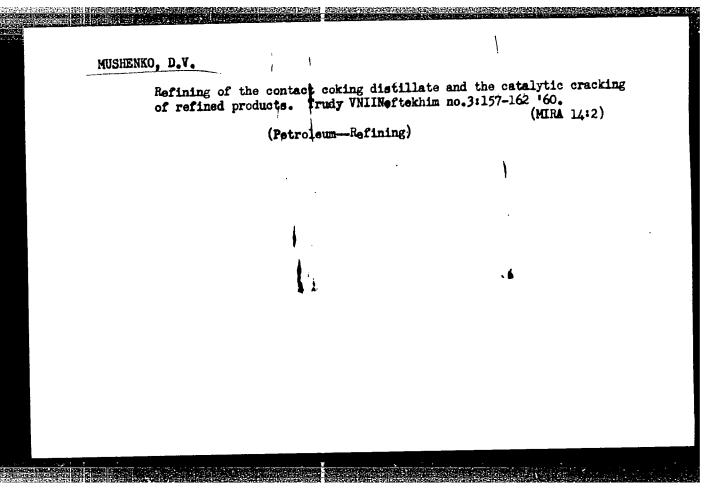
vyp. 3, 150-153)

TEXT: Mazout was subjected to contact coking on powdery activated carbon in the laboratory. With lower apparent density the activity of carbon was higher. In the coking experiments (475°C, volume rate 0.7  $hr^{-1}$ carbon addition 2 kg per kg of starting material) the gasoline yield decreased from 30.7 to 2% and the yield in the coking distillate (CD) from which gasoline had been removed increased from 10.6 to 76.3% if the apparent density of carbon was increased from 0.587 to 0.800. Catalytic cracking of CD proved that with CD that had been obtained from a less active catalyst, the gasoline yields are higher and the coke yields are lower; furthermore, it was found that the use of activated carbon in contact coking with subsequent catalytic cracking of CD shows no

Card 1/2

Contact coking of ma	zout on	S/081/61/000/012/022/028 B103/B202
advantages over the [Abstracter's note:	method in which non- Complete translation	
Card 2/2		

Conversion contact co	Conversion of fuel oil components and balance of elecontact coking. Trudy VNIINeftekhim no.3:154-156 *6		
	(Petroleum as fuel)		



Mushel	NKO, D.V.; LEVINA, M.I.; TAMMIK, M.E.					
	Hydrogenation of distillates obatined from the catalytic cracking					
	of Romashkino crude oil on a nickel-molybdenum catalyst. Trudy VNIINeftekhim no.3:163-172 '60. (MIRA 14:2)					
	(Petroleum—Refining) (Motor fuels)					
	(Hydrogenation)					
	·					
ANTENNASARAH KEMANCERIKAN PERE						

S/081/61/000/011/028/040 B103/B202

Mushenko, D. V., Levina, M. I., Tammik, M. E. AUTHORS:

Hydrogenation of the wide fraction of catalytic cracking of Romashki petroleum on catalysts with increased catalytic TITLE:

Referativnyy zhurnal. Khimiya, no. 11, 1961, 481, abstract PERIODICAL:

11M176 (11M176). ("Tr. Vses. n.-i. in-t neftekhim,

protsessov; vyp. 3, 1960, 173-177)

TEXT: Two new catalysts have been suggested: fluorine-nickel-molybdenum catalyst with the contents (in %): 0.5 F, 4.2 Ni, 6.8 Mo and chromiummolybdenum catalyst with 3.3 Cr and 5.6 Mo. They are used for hydrogenating a catalyzate from which benzene boiling up to 200°C has been removed and which had been obtained on cracking Romashki petroleum by using a powdery catalyst by the method of AZNII NP. The products were hydrogenated at a pressure of 100 atm and a temperature of 425°C. The product resulting from a two-stage processing of the strongly sulfurous Romashki petroleum was 76.1 % of pure commercial products, among them

Card 1/2

CIA-RDP86-00513R001135720003-9"

APPROVED FOR RELEASE: 03/13/2001

S/081/61/000/011/029/040 B103/B202

AUTHORS: Levina, M. I., Mushenko, D. V., Rysakov, M. V.

TITLE: Catalytic hydrogenation of sulfurous gas oils of catalytic and thermal cracking for the production of a Diesel oil and

a raw material for catalytic clacking

PERIODICAL: Referativnyy zhurnal. Khimiya, no. 11, 1961, 481, abstract

11**M**178 (11M178). ("Tr. Vses. n.-i. in-t neftekhim.

protsessov", vyp. 3, 1960, 178 - 182)

TEXT: It was found that by hydrogenating a mixture of two kinds of the gas oil of catalytic cracking and the Diesel oil (from Devonian petroleum) in the ratio 1: 1 a high-quality summer Diesel oil can be obtained by means of a Co-Mo catalyst at 30 atmospheres excess pressure. When hydrogenating the gas oil fractions 200 - 350°C and 215 - 490°C of catalytic cracking and of the cracking residue (from the same petroleum) raw materials for catalytic cracking can be obtained at 50 - 100 atmospheres excess pressure whose properties are superior to those of raw materials obtained by direct distillation. Abstracter's note: Complete translation.

VISHNEVSKIY, N.Ie.; MAYOROV, D.M.; MUSHENKO, D.V.

Hydrogenation of fuel oil under a pressure of 100 atm. Trudy
VNIIMeftekhim no.3:183-186 '60. (MIRA 14:2)

(Petroleum as fuel) (Hydrogenation)

24828

5/081/61/000/011/135/04 0110/8001

5 3300

AUTHORS:

Telegin, V. G., Kobelev, V. A., Mushenko, I. V.

TITTE:

Alkylation of propylene by isobuter in the presence of

hylrofluoric acid

PERIODICAL:

Referativnyy zaurnal. Maniya, or. 11. 1. 1. 1. 1. 11M217 (11M217) (Tr. Vses. n.-i. in-t reft dollar, prot entrov,

1960, vyp. 3, 187-192)

INTO. The alkylation of propylene by isobutant in the pro-new of the us been studied. Commercial 98, isobutone and propplete. She find y denydration of icopropancl, were used for the surpose. Inhydroun nydrofluoric acid containing 98.5% of HF and 1. p of De, was taken as a catalyst. In their experiments, the authors varied the reaction temperature between to and 44°C, the duration of confect from to to minutes. the molar ratio of isobutane to propylene from 12.5.1 to 1.6.1. and the degree of HF dilution by water at a constant pressure of that. The quality of the alkylate is hardly affected by temperature, whilet its yield increases with a rise in temperature (at 15°3 it is 1.4) referred to

Card 1/2

21,828 3,981/61 (1111/35/54 3... 811c/5/61

Alkylation of propylene by ...

propylene, and at 35-40°C it is 235-2470). When the dustion of contact is prolonged, the yield in alkylate rises, and the composition changes in that the amount of primary products (2,3-dimethyl pentane, in reduced, while that of secondary products (2,4-trimethyl pentane, increases, Raising the molar ratio from 1.6 to 1.7 results in an increase of the alkylate yield from 166 to 244' referred to propylene, or the content of aviation alkylate in the alkylate from 85.3 to 25.2, of the content of 2,2,4-trimethyl pentane in the alkylate from 16.0 to 13.7, and or the octane number from 67.6 to 91.1 (noter method). Dilution of HI by later lowers its catalytic activity and fivors fluction tion and colymerization reactions. Accumulation of resin in the acid up to 2 has a favorable influence on the yield and properties of blkylate. Sprimum conditions for applying the new procedure have been proposed on the basis of the test results. Abstructor's note: Complete translation.

Card 2/2

26195 S/081/61/000/012/021/028 B103/B202

5.3300

AUTHORS: Telegin, V. G., Kobelev, V. A., Mushenko, D. V.

TITLE: Alky

Alkylation of butylenes by means of isobutane in the

presence of hydrogen fluoride

PERIODICAL:

Referativnny zhurnal. Khimiya, no. 12, 1961, 524, abstract 12M162 (Tr. Vses. n.-i. in-t neftekhim. protsessov, 1960,

vyp. 3, 195-194)

TEXT: A mixture consisting of 44% of isobutylene and 56% of n-butylenes was alkylated by means of commercial 90% isobutane in the presence of a catalyst (98.8% HF + 1.2%  $SO_2$ ), at a temperature of  $30^{\circ}$ C, a pressure of

10 at overpressure, and a volume ratio HF: hydrocarbons of 1: 1. The experiments showed that the alkylate yield increases from 177 to 193% with an increase of the molar ratio isobutane: butylene from 4: 1 to 10.8: 1. In this case lighter alkylates are obtained with a low final boiling point. This method warrants - as compared to the sulfuric-acid alkylation of the same starting material - a higher yield (by about 10%)

Card 1/2

X

Card 2/2

21,829

S/081/61/000/011/ 36/040 B110/B201

5 3300

AUTHOR:

Mushenko, D. V.

TITLE:

Alkylation of amylenes and hexylenes by isobutane

PERIODICAL:

Card 1/2

Referativnyy znurnal. Knimiya, no. 11, 1961, 486, abstract 11M218 (11M218)(Tr. Vses. n.-i. in-t neftekhim. protsessov,

1960, vyp. 3, 195-209)

TEXT: Alkylation of the pentane-amylene and hexane-hexylene fractions of thermal cracking by isobutane in the presence of  $\rm H_2SO_4$  has been

studied under the following conditions: temperature,  $10^{\circ}\text{C}$ ; pressure, studied under the following conditions: temperature,  $10^{\circ}\text{C}$ ; pressure, 10 At; duration of contact, 40 min; ratio of isobutane to olefin 10 At; duration of the following temperature and the fraction, the yield of alkylate was 160-1650 referred to amylene, amylene fraction, the yield of alkylate was 160-1650 referred to amylene, and that of aviation alkylate with a final boiling point of  $180^{\circ}\text{C}$  was and that of aviation alkylate with a final boiling point of  $180^{\circ}\text{C}$  was 143-148% at an  $12^{\circ}\text{C}$ 0 concentration of 185-98%. The octane number of pure aviation alkylate as found by the motor method was  $12^{\circ}\text{C}$ 1. For the hexane-hexylene fraction in the presence of  $12^{\circ}\text{C}$ 2. The yield of

24827

s/081/61/500/011/134/045

B110/B201

5 3300

Mushenko. D. V.

TITLE:

AUTHOR:

Alkylation of butylenes by isopentane

: ERIODICAL:

Referativnyy zhurnal. Khimiya, no. 11. 1961, 485-486. abstract 11M216 (11M216) (Tr. Vses. nei. in-t reftek.im.

protsessov, 1960, vyp. 3, 210-2181

TEXT: For the purpose of enlarging the resources for high octane-rubber components and making economic use of excess amounts of isogentane from catalytic cracking units, the suggestion is made to use isopentane for butylene alkylation. Commercial isopentane [95], isopentane, 4 n-pentane, and 1,5 n-butane) and a butylene mixture consisting of 40 parts of isobutylene and 60 parts of n-butylene were used here. Alkyl tion was performed at a temperature of 10°C. a pressure of 10 At. a contact duration of 40 minutes, and a weight ratio of isopentane to butylene > 0.514in the presence of 86-98%  $\rm H_2SO_4$ . The yield of akylate was  $\rm CoC+2$ 

referred to butylene, and that of aviation alkylate with a final boiling

Jard 1/2

MAYOROV, D.M.; MERKULOVA, O.P.; MUSHENKO, D.V.; TEODOROVICH, V.P.

Selection of materials for the units performing the direct hydrogenation of higher fatty acids. Khim.prom. no.3:210-212 Mr '61.

(MIRA 14:3)

1. Vsesoyuznyy nauchno-issledovatel'skiy institut neftekhimicheskikh protsessov.

(Acids, Fatty) (Hydrogenation)

KOBELEV, V.A. [deceased]; MUSHENKO, D.V.; TELEGIN, V.G.; TEREBILOVA, M.A.

Decomposition of fluorides and removal of fluorine from alkylates.
Trudy VNIINeftekyim no.3:214-218 '60. (MIRA 14:2)

(Alkyl fluorides) (Fluorine)

KOBELEV, V.A. [deceased]; MUSHENKO, D.V.; TELEGIN, V.G.; TEREBILOVA, M.A.

Removal of fluorine from alkylates by means of copper-aluminum alloys.

Trudy VNIINeftekhim no.3:219-222 '60. (MIRA 14:2)

(Alkyl fluorides) (Fluorine)

MUSHENKO, Dmitriy Vasil'yevich; LEVINA, Mariya Iwanovna; LEVIN, S.Z.,
nauchmyy red.; SEGAL', Z.G., ved. red.; SAFRONOVA, I.M.,
tekhn. red.

[Petroleum refining without mazut] Bezmazutnaia pererabotka
nefti. Leningrad, Gos.nauchno-tekhn.izd-vo neft. i gornotoplivnoi lit-ry, 1961. ll6 ps. (MIRA 15:2)
(Petroleum—Refining) (Mazut)

S/064/61/000/003/00e/009 B101/B203

AUTHORS:

Mayorov, D. M., Merkulova, O. P., Mushenko, D. V.,

Teodorovich, V. P.

TITLE:

Selection of material for the apparatus of direct hydro-

genation of higher fatty acids

PERIODICAL: Khimicheskaya promyshlennost, no. 3, 1961, 62-64

TEXT: In connection with the development of the production process of higher aliphatic alcohols by direct hydrogenation of fatty acids, the problem of selecting suitable corrosion-resisting material for the apparatus arose. The present paper reports on corrosion tests. Two methods were applied: 1) To select the material for the hydrogenation vessel and the separator, metal specimens were tested directly in the reaction vessel of the hydrogenation plant at 340°C, 300 atm, or in the separator. After testing for 1978 hr, the following corrosion rates (mm per year) were found: CT -20 (St-20) steel 7.0; 1x13 (1kh13) steel 0.4; 1x18H9T (1kh18N9T) steel 0.002; 1x18H12M2T (1kh18N12M2T) 0.01; 3M-435 (EI-435) 0; industrial aluminum 0.08. 2) The material for the heat exchangers was Card 1/5

S/064/61/000/003/008/009 B101/B203

Selection of material for ...

tested by heating the specimens with the fatty acids (C7 - C20) in an autoclave at 5 atm hydrogen pressure up to  $150^{\circ}$ C. For less important parts, they were heated in a thermostat to  $50^{\circ}$ C. Table 5 gives the experimental data (mm per year). Testing of the electrically welded seams (analysis of electrodes, Table 4) by method 2 showed that the seams were also resistant. In a test plant, various metals were tested for corrosion resistance during hydrogenation of C7 - C9 and C10 - C16 acids at 230°C and 300 atm. It was found that steels with 18-20% Cr were sufficiently resistant. Test results of metals and welding seams at 1000 and 150°C in an autoclave are given in Table 8. The widely used 1Kh18N9T steel proved to be suitable. Testing for intergranular corrosion (t =  $230^{\circ}$ C, p = 300 atm) of untreated and thermally treated specimens of this steel showed corrosion rates of 0.001 mm/year in both cases. A hydrogenation apparatus made of this steel has been operating 4 years now. Low-alloy steels (EI-579) are suited for temperatures up to 50°C. For temperatures between 70 and 150°C, the steel must contain at least 13% of chromium. Aero-fireclay bricks proved to be stable in tests during 200 hr at 100 and 150°C in the presence of C10 - C16 acids. There are 9 tables Card 2/5

5/064/61/000/003/008/009 B101/B203 Selection of material for .... and 1 Soviet-bloc reference. ASSOCIATION: Vsesoyuznyy nauchno-issledovatel'skiy institut neftekhimicheskikh protsessov (All-Union Scientific Research Institute of Petrochemical Processes) Таблица 4 Химический состав наплавленного металла электродов, использованных для сварки сталей 1X18Н9Т и 1X18Н12М2Т (%) 4 Тип наплав-лениого металла Cr Ni Nb С Si Mn Legend to Table 4: 1) Type of metal welded-on. 2) TsL-11. 3) ENTU-3. 4) KTI-5. 5) TsT-15. Card 3/5

Selection of material for ...

S/064/61/000/003/008/009 B101/B203

<b>Д</b> Метвля	9,Температура			<b>.</b> ,Температура	
	202	150°	A Металл	50°	150°
3 CT- 20	0,35	4,0	4ри-943	0,002	0,00
УЭИ-579	.0.007	1,9	оАлюминий техни- ческий	0.002	0.02
1Χ18H9T	0.002	0.07	Conan Al+Mg .	0.02	0,03
> 1X18H12M2T .			имедь	_	0,03
ЭИ-432	0,0006	0,003	Патунь	<b> </b> -	0,02

Table 5

Legend to Table 5: 1) Netal. 2) Temperature. 3) St-20. 4) EI-579.
5) 1Kh13. 6) 1Kh18N9T. 7) 1Kh18N12M2T. 8) EI-432. 9) EI-943.
10) Industrial aluminum. 11) Alloy. 12) Copper. 13) Brass.

Card 4/5

MUSHENKO, D.V.; VISHNEVSKIY, N.Ye.; MAYOROV, D.M.

Organizing the production of methyl ethyl ketone. Khim.i tekh.topl.i masel 6 no.8:66-67 Ag '61. (MIPA 14:8)

1. Vsesoyuznyy nauchno-insledovatel'skiy institut neftekhimicheskikh protsessov. (Ketone)

S/065/61/000/012/001/005 E075/E135

AUTHORS: Mushenko, D.V., Levina, M.I., Tammik, M.E.,

Mochalovskaya, A.P., Semenova, V.V., and Zimina, A.V.

TITLE: Pilot-plant deresinification of crude oils by

contact process

PERIODICAL: Khimiya i tekhnologiya topliv i masel, no.12, 1961.

TEXT: The contact process for deresinification of crude oils developed by VNIINeftekhim in 1953-1955 was tested in a pilot plant to obtain data for industrial planning. The plant consisted of a heat-exchanger, capable of heating the oil to 430-450 °C and 70-30% vaporization, and a refractory brick-lined reactor suitable for operation at temperatures up to 1000 °C. An improved iron-containing contact catalyst was prepared for the experimental runs in a catalyst factory, in the form of cylindrical pellets (5 mm²). The reactor was charged consecutively with a 15 cm layer of 25 x 25 mm Raschig rings, 10 cm layer of 10 x 10 mm Raschig rings, the first 125 cm-high layer of the contact catalyst, an

Card 1/4/

MUSHENKO, D.V.; VISHNEVSKIY, N.Ye.; GUSHCHEVSKIY, A.B.; CHERNOUSOV, N.P.

Selecting a reactor for the production of isobutysulfuric acid.

Khim.prom. no.4:271-273 Ap 162. (MIRA 15:5)

1. Vsesoyuznyy nauchno-issledovatel skiy institut neftekhimicheskikh protsessov i Leningradskiy filial Vsesoyuznogo nauchno-issledovatel skogo i konstruktorskogo instituta khimicheskogo mashinostroyeniya.

(Isobutyl sulfate) (Chemical reactors)

IGONON, P.G., inzh.; SVITKIN, V.V., inzh.; MITROFANOV, M.G., kand.tekhn.nauk; SLEPTSOV, Yu.S., inzh.; KOLOZHVARI, A.A., inzh.; PASHENKO, M.A., inzh.; ZHIVOLUPOVM.A., inzh.; Prinimali uchastiye: MUSHENKO, D.V.; TSYSKOVSKIY, V.K.; SHCHEGLOVA, TS.N.; FREYDIR, B.G.; PYL'NIKOV, V.I.; LEVINA, M.I.; LEVIN, A.I.; LUR'YE, Ye.I.; BAYKINA, T.A.; UDOVENKO, S.A; MARCHENKO, T.A.

Effect of the method of liquid paraffin oxidizing on the yield and quality of the obtained fatty acids. Masl.-zhir.prom. 28 no.11:20-23 N \*62. (MIRA 15:12)

1. Groznenskiy nauchno-issledovatel'skiy neftyanoy institut (for Igonin, Svitkin, Mirtofanov, Sleptsov, Kolozhvari, Pashenko, Zhivolupov).

2. Vsesoyuznyy nauchno-issledovatel'skiy institut neftekhimicheskikh protsessov (for Mushenko, TSyskovskiy, Shcheglova, Freydin, Pyl'nikov, Levina, Levin).

3. Lengiprogaz (for Lur'ye, Baykina).

4. VNIISINZh (for Udovenko, Marchenko).

(Paraffins) (Acids, Fatty)

3/080/62/035/010/009/012 D204/D307

Roskin, Ye., Rushenko, J.V., Vishnevskiy, N.Ye.,

karpenlo, U.J. and Dergachev, R.D.

study of the effects of hydrodynamic conditions on : نظاء ما الأداللة.

the polymerization of acrylonitrile TITLL:

Lhurnal pril: ladnoy khimii, v. 35, no. 10, 1962,

PERCONTONL:

The present work was concerned with the effects of ctirring on the polymerization reactions of acrylonitrile in aqueous solutions (7%), owing to the increasing importance of such polymers in the production of artificial fibers. The reactions were carried out under arron in a stainless stable autoclasse with stirring out under argon in a stainless steel autoclave, with stirring (2800 rpm, Re being 6000 or 46000), at 15 - 450C, under isothermal conditions. Similar experiments were carried out under static conditions. Similar experiments were carried out under static conditions in air and in argon when and available acid were used as ditions, in air and in argon. Rino4 and oxalic acid were used as initiators. In stirred solutions, after 15 min reactions, the initiators. In stirred solutions, after 15 min reactions and fell to yields increased from ~ 20% at 1500 to ~ 60% at 300 and fell to

Card 1/2

Study of the effects ...

3/080/62/035/010/009/012

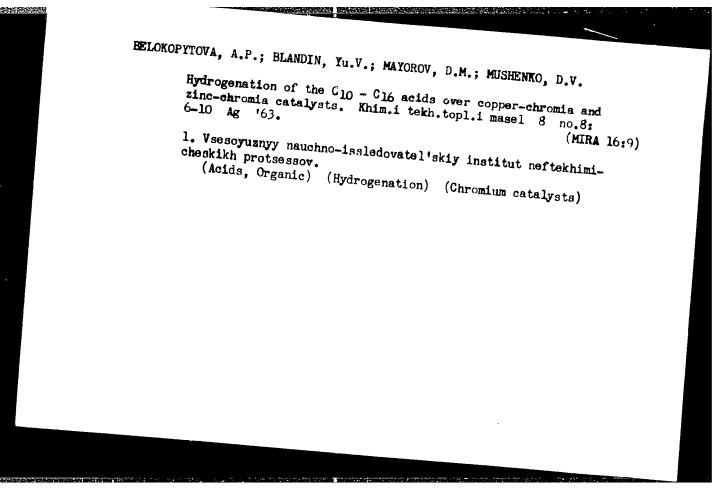
~ 47% at 45°C. The corresponding figures after a 40 min reaction were ~ 49, 70 and 500 respectively, tending to be always slightly lower in the more intensively stirred solutions. Yields of statically carried out reactions under argon were on the average ~ 10% higher than the above, and were higher still when the polymerization took place (still without stirring) in air. In small amounts, oxygen improves the yields, but reverses its action and even stops the reaction completely when introduced in large amounts, e.g. by stirring in systems open to the atmosphere. There are 5 figures and 1 ASSOCIATION:

Leningradskiy tekstil nyy institut im. S.M. Kirova (Leningrad Institute im. S.M. Kirov); Vsesoyuznyy nauchno-issledovatel'skiy institut neftekhimicheskikh protsessov (All-Union Scientific Research Institute of retrochemical Processes)

SUBLITT D:

July 5, 1961

Card 2/2



MUSHENKO, D.V.; VISHNEVSKIY, N.Ye.; DERGACHEVA, R.D.

Decomposition and hydrolysis of isobutylsulfuric acid.

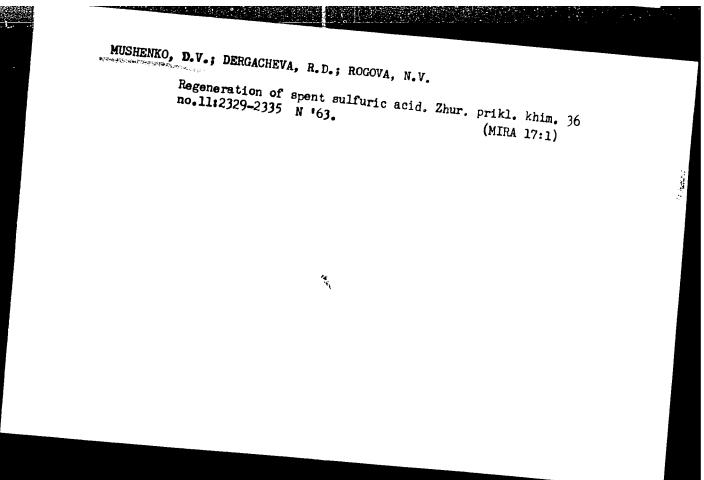
Zhur. prikl. khim. 36 no.9:2038-2044 D '63. (MIRA 17:1)

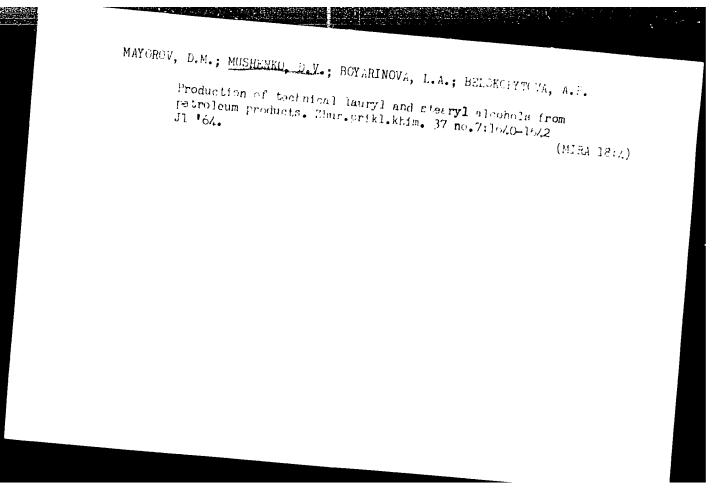
1. Vsesoyuznyy nauchno-issledovatel'skiy institut nefte-khimicheskikh protsessov.

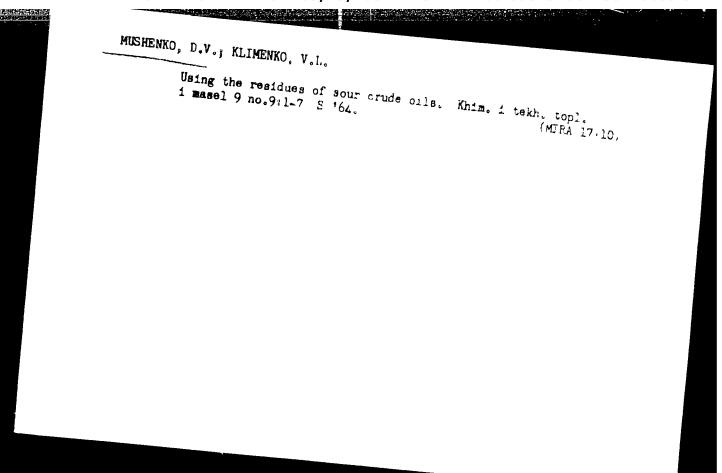
MUSHENKO, D. V.; VISHNEVSKIY, N.Ye.; DERGACHEVA, R.D.; MALOV, Yu.I.

Preparation of concentrated isobutylene. Zhur. prill. khim.

l. Vsesoyuznyy nauchno-issledovatel'skiy institut nefte-







MUSHENKO, D.V.; GVOZDOVSKIY, G.N.; SEMENOVA, V.V.

Liquid-; hase oxidation of the pentane-hexane fraction of straight-run gasoline with recycling of the intermediate oxidation products. Khim.i tekh.topl. i masel 10 no.ll;

1. Vsesoyuznyy nauchno-issledovatel skiy institut neftekhimi... (MIRA 19:1) cheskikh protsessov.

"APPROVED FOR RELEASE: 03/13/2001

EWT(d)/EWP(f)/EPF(n)-2/EWP(v)/T-2/EWP(k)/EWP(h)/EWP(1)/ETC(m)-6 AP6009924 SOURCE CODE: UR/0413/66/000/004/0118/0119

INVENTOR: Korotkov, F. A.; Mushenko, G. I.; Dobrynin, A. N.; Sokolov, Ye. A.

ORG: none

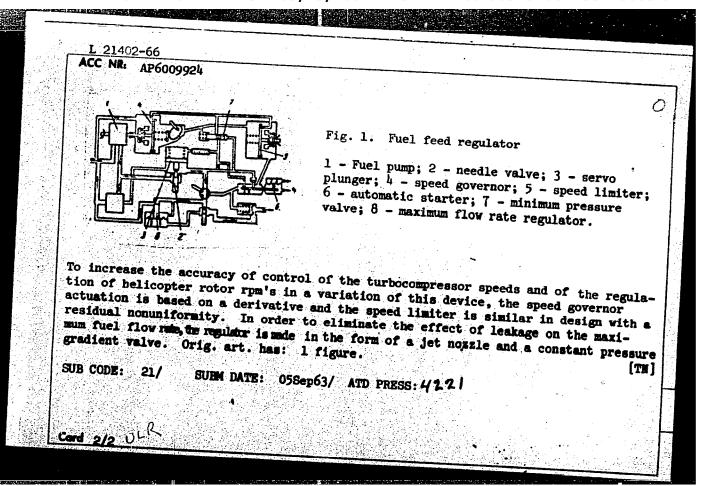
TITLE: Fuel feed control device for gas turbine engines. Class 46, No. 179127

SOURCE: Izobreteniya, promyshlennyye obraztsy, tovarnyye znaki, no. 4, 1966,

TOPIC TAGS: gas turbine installation, engine turbine system, turbine fuel system,

ABSTRACT: The proposed fuel feed regulator contains a fuel pump which feeds the fuel to a metering needle valve with a servo-plunger whose cavities are connected by a duct. The device also includes an engine speed limiter and speed governor, an automatic starter, and a minimum pressure valve which are located parallel to the constant pressure-gradient valve which maintains a constant fuel pressure drop across the needle valve (see Fig. 1). To increase the accuracy of control and reduce the weight and size, one of the plunger cavities is directly connected to the same line through a jet nozzle and a throttle unit. The duct between the cavities is also connected to the control element of the starter and through the minimum pressure valve to the sensing element of the speed limiter and speed governor. Cara 1/2

UDC: 621.438-543.3-531.9

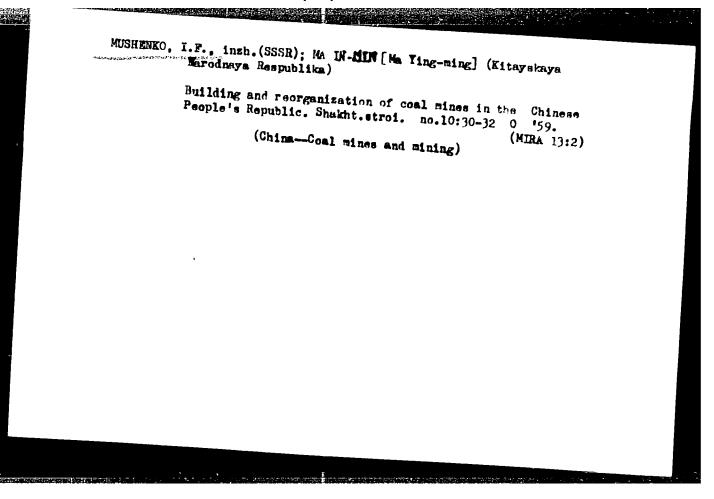


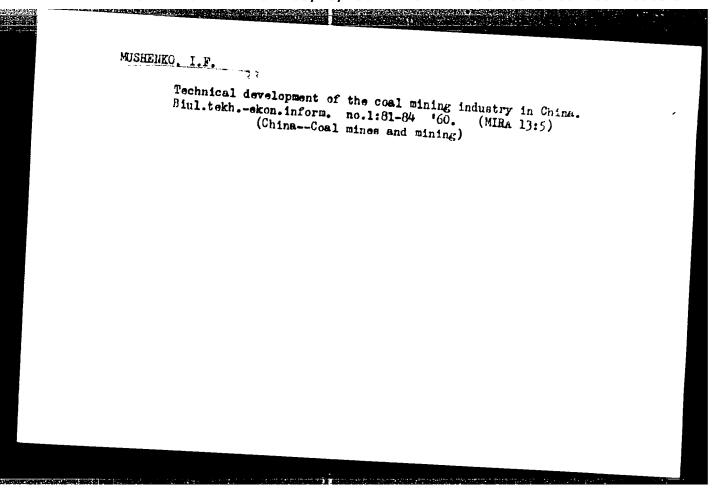
MUSHRUKO. Iyan Fedorovich; AFONINA, G. [Afonina, H.], red.; MATUSEVICH, S., tekhn.red.

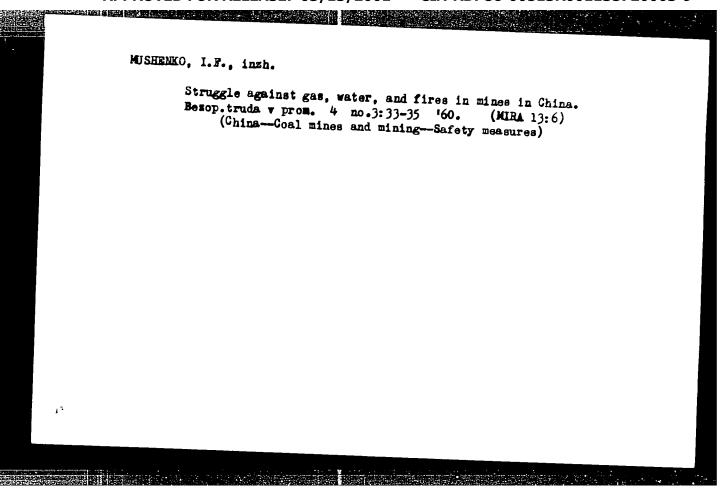
[Coal mining in the Chinese People's Republic] Vydobutok vugillia v Kitais'kii Narodnii Respublitai. Kyiv, Derzh.vyd-vo tekhn.ltt-ry UHSE, 1959. 126 p.

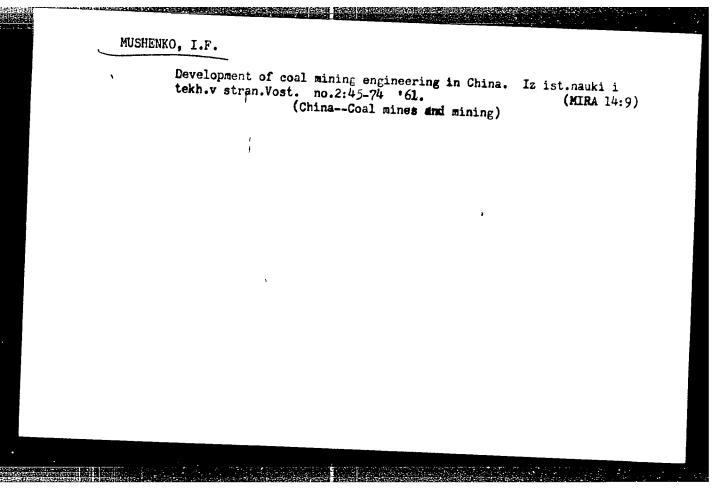
(China--Coal mines and mining)

(MINA 13:8)

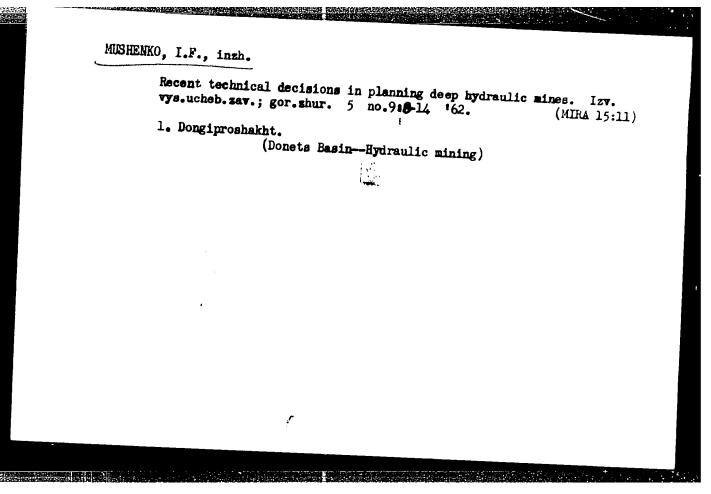


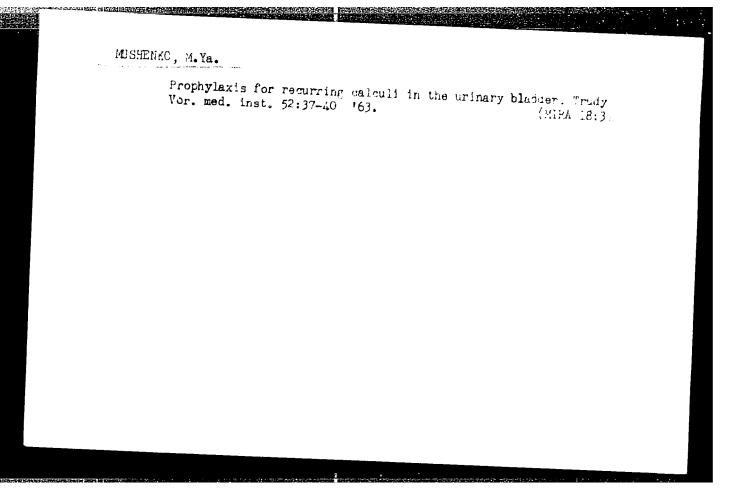


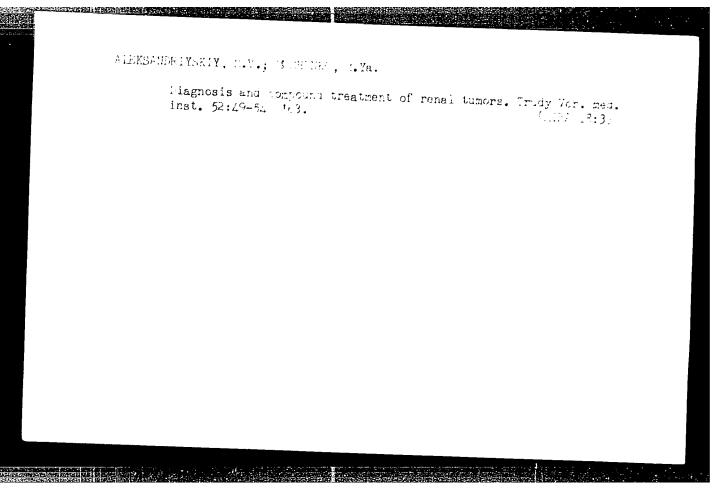




Concerning the plan for an over-all reorganization of Stalinugol' Combine mines. Ugol' Ukr. 5 no.2:8-10 F '61. (MIRA 14:3)
1. Stalingiproshakht.
(Donets Basin-Coal mines and mining)







ACCESSION NR: AT4010227 .

\$/3056/63/000/000/0071/0075

AUTHOR: Mushenko P. M.

TITLE: The accuracy of a thermogradientograph on a meteorological tower

SOURCE: Issledovaniye nizhnego 300-metrovogo sloya atmosfery\*. Hoscow, 1963,

TOPIC TAGS: meteorology, temperature measurement, thermal gradient, thermo-

ABSTRACT: After discussing the maximal permissible error in the use of the thermogradientograph (TGG), the author points out that instrument precision depends both on the rated precision and the precision of correction. Equations for determining the precision mathematically and methods for improving the precision of correction are developed. Data obtained on a meteorological tower in 1961 are given for the errors on the + 3° and + 1.5° scales of a TGG. The experimental data shows that in practice the TGG error does not change during conversion from one scale to another, amounting to an average of + 0.1°. Improvements in precision can only be obtained by repeating the first stage of correction and by increasing the number of readings. "F. Ya. Klinov, B. Ya. Tolstobrov, L. Ye. Cord

MUSHENKO, P.M.

Comparison of the characteristics of the atmospheric turbulence recorded on an automatic integral pulsimeter (AIP) and those obtained by the method of instantaneous smoke exhausts. Trudy Len. gidromet. inst. no.15:226-228 163.

Experimental studies of the dispersion of pollution from instantaneous point sources. Ibid.:279-238 (MIRA 17:1)

APPROVED FOR RELEASE: 03/13/2001 CIA-RDP86-00513R001135720003-9"

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ACC NR: AR6032145	
300RGE CODE: UR/0169/66/000/0	06/B016/B016
AUTHOR: Bekryayev, V. I.; Vaksenburg, Z. B.; Mushenko, P. M.	
TITLE: Air-pollution study in the region of the Baltic GRES (State Regions Plant)	al Power
SOURCE: Ref. zh. Geofizika, Abs. 6B126	;
REF SOURCE: Sb. rabot Tallinsk. gidrometeorol. observ., vyp. 3, 1965, 47-4	9
TOPIC TAGS: atmospheric admixture, sulfur dioxide, air pollution, ATMOS CONTRACTION, SULFUR COMPOUND	PHERIC
ABSTRACT: Some theoretical schemes for computing the expansion of atmosphe impurities are analyzed on the basis of observation data of the contents of dioxide and dust in the atmosphere.	ric sulphur
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L 04205-67 EWT(1) ACC NR AR6000718 SOURCE CODE: UR/0124/65/000/009/B106/B106 AUTHOR: Mushenko, P. M. TITLE: Estimation of the water content of cirrus clouds SOURCE: Ref. zh. Mekhanika, Abs. 9B699 REF SOURCE: Tr. Leningr. gidrometeorol. in-ta, vyp. 22, 1964, 56-66 TOPIC TAGS: atmospheric condensation, atmospheric cloud, atmospheric water, vapor condensation, exhaust gas, atmospheric temperature ABSTRACT: At the present time there is meager information on the water content of cirrus clouds. According to the indirect estimates of Veykman, it is 0.1 g/m3; according to the data of Camp, based on values of the visibility range, it is 0.03 g/m3. Minervin's measurements in crystalline altostratus clouds gave values of 0.003-0.002 g/m3; it can be assumed that the water content has lower values in cirrus clouds. The episodic measurements of the water content in cirrus clouds by V. S. Kozhazin gave values of 0.002-0.005 g/m3. The work gave an estimate of the water content in the condensation trails of aircraft (clouds of type Co tractus). The possibility of comparison of the water content of condensation trails and cirrus clouds is pointed out. The distribution of the water content in a condensation trail is obtained by means of expressions for the specific water content q and the absolute water content w urd 1/2

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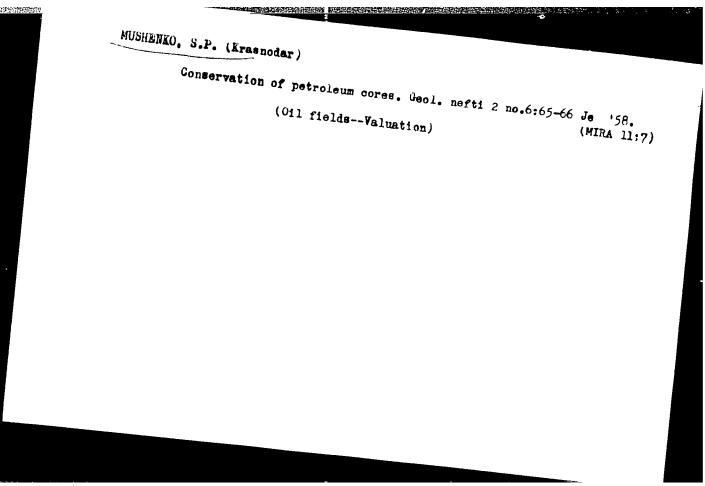
$$q = \frac{\Delta q_0}{\Delta t_0} (t - t_h) + q_h - \frac{\mu}{M} \frac{E(t)}{p_h}$$

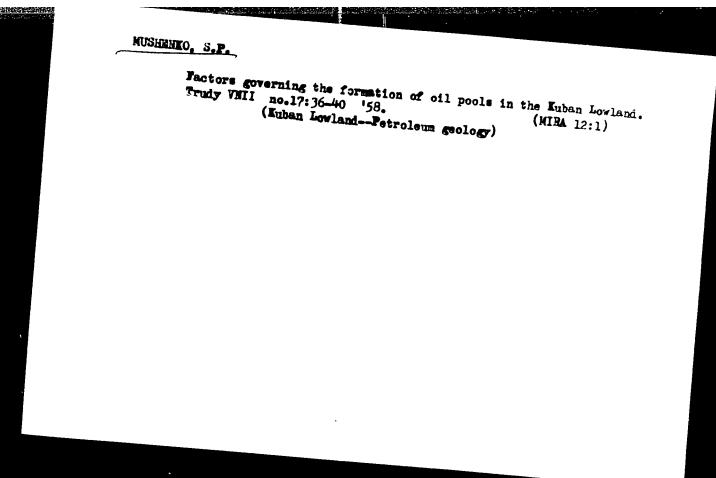
$$\omega = \frac{\Delta l_0}{R_h (273 + t)},$$

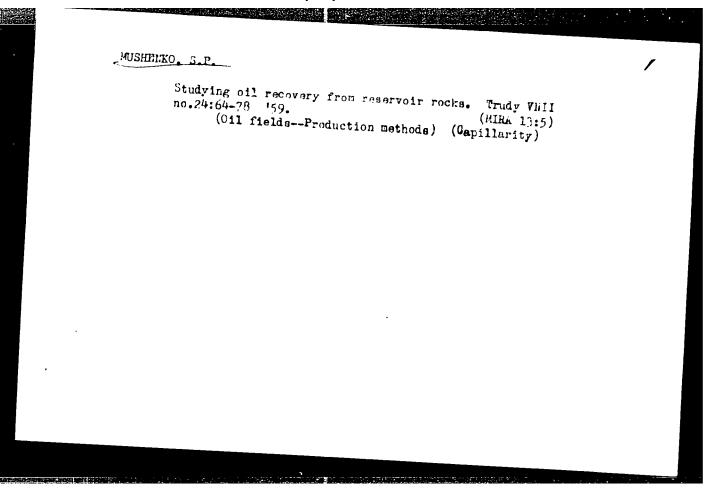
where  $\Lambda q_0$  is the excess difference between the moisture contents;  $\Delta t_0$  the excess temperature difference;  $t_0$ ,  $t_k$ , and t the temperatures in the initial cross section of the jet, in the medium surrounding the jet, and at any point in the jet;  $p_h$  at a surrounding the jet, and at any point in the jet;  $p_h$  and  $p_h$  the atmospheric pressure;  $p_h$  the saturation pressure at temperature t;  $p_h$  and  $p_h$  the molecular weights of water and the water content. The method of  $p_h$  the  $p_h$  and  $p_h$  the calculated values the jet. Within the space occupied by the condensation trail, the calculated values of the water content were from 0.071 to 0.003  $p_h$  (water) and 0.151 to 0.004  $p_h$  of the water content were from 0.071 to 0.003  $p_h$  (water) and 0.151 to 0.004  $p_h$  of the vertical extent of natural circus clouds is one order of magnitude (ice). Since the vertical extent of natural circus clouds is concluded that the values of greater than the thickness of condensation trails, it is concluded that the values of water content in circus clouds will be considerably lower than the calculated values.

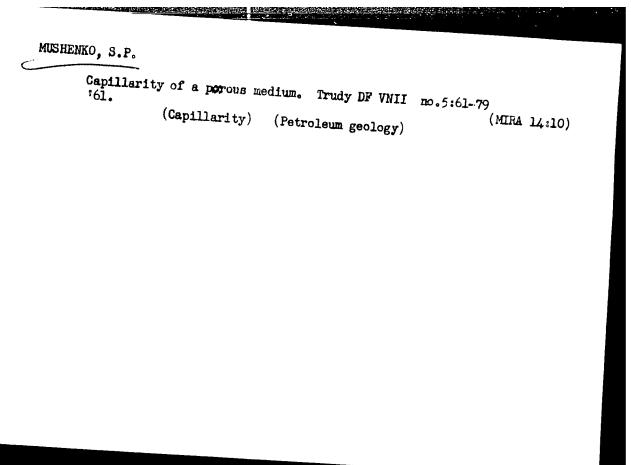
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Using a method	a torsion balance if	for determining for Trudy KF VNII	interfacial tens no.5:80-83 '6	ion by the l. (MIRA 14:10)		
	(Surface tension)					

LYAFISHEV, M.B.; MUSHENKO, S.P.

Studying the capillarity of grained rocks. Izv. vys. ucheb. zav.; neft'i gaz 6 no.2:34-39 '63. (MIRA 16:5)

1. Vsesoyuznyy zaochnyy politekhnicheskiy institut. (Capillarity) (Oil sands--Permeability)